CO₂ Capture Plants

With capture plants from Union Engineering, carbon dioxide can be captured from any gas stream based on the combustion of fossil fuels, including but not limited to coal, heavy fuel oil fired steam boilers, and natural gas fired combustion engines.

Moreover, the technology can be used to capture carbon dioxide from non-power generation sources, like lime kilns.

The capture plants from Union Engineering are based on the most well-proven absorption technology currently available on the market, namely high concentrated monoethanolamine (MEA). MEA is a primary amine that reacts readily with carbon dioxide. Since the reaction is purely chemical absorption, it works well with gas streams having low partial CO₂ pressure, as is the case for flue gases.

Once the carbon dioxide is captured in the MEA solution it is transferred to a stripping system. Here it is again released from the MEA solution by increasing the temperature of the solution to a point where the chemical reaction that took place in the absorber is reversed.

Having started as a gas with a low concentration of carbon dioxide (depending on the type of fuel used the CO₂ will be in the range of 3% to 30%), the gas being released from the stripper is a highly concentrated stream containing roughly 99% pure carbon dioxide. This stream can either be used directly in gaseous form or be further purified and liquefied to meet the strictest requirements for food and beverage grade carbon dioxide in accordance with specifications from regulators like the International Society of Beverage Technologists (ISBT).

Purification column is the final purification step, consisting of a distillation column which enables separation/blow-off of non-condensable gasses, thereby reducing O₂ content in the final product to max. 5 ppm (v/v) and obtaining corresponding CO₂ purity of higher than 99.99% (v/v).

The electrical system for the CO₂ generating plant consists of a combined MCC and control panel. From the control panel, which comprises the latest PLC technology, the plant is operated and monitored, ensuring easy and continuous trouble-free operation.

The plant is started by an automatic start sequence and the operation is fully automatic. The entire process is easily surveyed on the operator panel, showing the status of all drives, readings of all transmitters and alarm warnings, which will also be indicated by audible alarm.

All instruments installed on the skids are wired to junction boxes or remote I/O boxes and tested in our workshop prior to shipment, thus reducing installation and commissioning time on site.

The plants are designed for high efficiency, availability and reliability through components selected for long life and 24/7 operation.
The plant is based on extraction of CO₂ from an existing flue gas source resulting in significantly operating saving compared to traditional CO₂ Generation Plants. Basically any available flue gas source can be used the MEA solvent is continuously purified by means of a unique system allowing for high O₂ feed gas content which in other installations would result in excessive solvent degradation and plant corrosion. No use of inhibitors is needed and the solvent used constitutes a 35 w/w % MEA solution which is easily available.

The flue gas is directed to a flue gas scrubber, in which the gas is cooled and water condensed. Any SO₂ present in the flue gas will be removed by means of a chemical reaction with sodium carbonate (soda ash). The soda ash is automatically added to the scrubbing water by means of pH control.

After cooling and scrubbing, the gas is led via an exhauster through an absorber, in which the gas flows counter-current to the MEA solution flow. By chemical reaction, the MEA solution absorbs the CO₂ from the flue gas. The MEA solution containing the absorbed CO₂ (referred to as rich MEA solution) is first pressurised and heated in a heat exchanger and then led to the NOxFlash column. Here most of the contaminants are removed from the rich MEA solution by flashing to the absorber pressure. Further heating is added to the bottom of the NOxFlash column for further reduction of the contaminants in the MEA solution. This optimises the process yield to the best possible CO₂ product without any use of expensive chemicals (Union patent pending).

The rich MEA solution is pumped to a stripper, where the CO₂ is released from the MEA solution by means of the combustion heat generated in the MEA heater. The CO₂ depleted MEA solution (referred to as lean MEA solution) is recycled to the absorber. Prior to liquefaction, the gas is dried to a dew point of approx. -60°C (10 ppm v/v H₂O) in the dehydration. Regeneration is done automatically by electrical heating and use of dry purge gas from the CO₂ condenser. Traces (if any) of acetaldehyde are also removed in the dehydrator. The CO₂ gas then passes through an activated carbon filter for removal of any odour substances.

To remove the last non-condensable gases, the CO₂ gas first passes a reboiler in the purification system (type PUR-D). It is then condensed at a temperature of approx. -27°/-21°C in a CO₂ condenser, where the non-condensable gases are purged off. Finally, the liquefied CO₂ is led through the distillation column to an insulated storage tank.

A refrigeration unit, controlled by the CO₂ pressure in the CO₂ condenser, supplies the matching refrigeration capacity. The liquid CO₂ is stored under a pressure of approx. 15-18 bar(g) and a corresponding temperature of approx. -27°/-21°C. During a non CO₂ production period, the refrigeration unit is able to operate independently of the rest of the CO₂ plant in order to maintain the correct CO₂ storage tank temperature/pressure.

The CO₂ produced has a purity higher than 99.99% (v/v) and fulfils quality standards as a food/beverage ingredient.